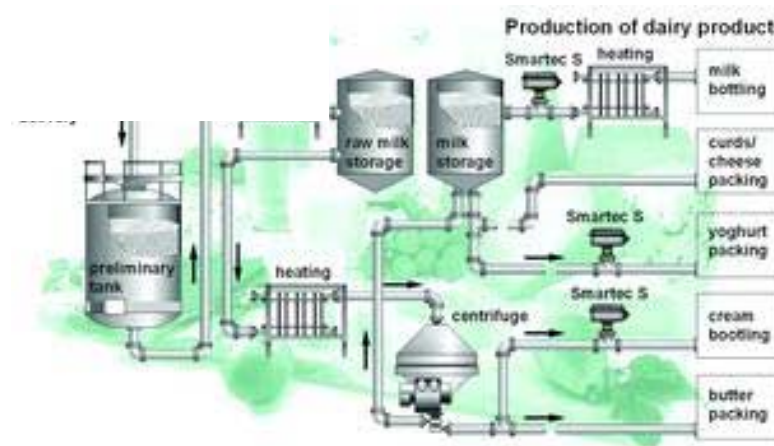
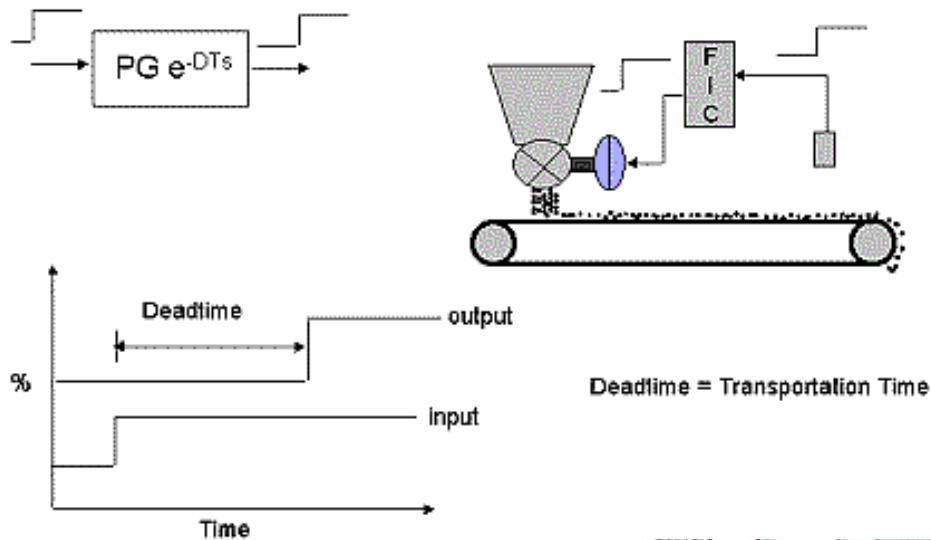


# Lecture 9 - Processes with Deadtime, IMC

- Processes with deadtime
- Model-reference control
- Deadtime compensation: Dahlin controller
- IMC
- Youla parametrization of all stabilizing controllers
- Nonlinear IMC
  - Dynamic inversion - Lecture 13
  - Receding Horizon - MPC - Lecture 12

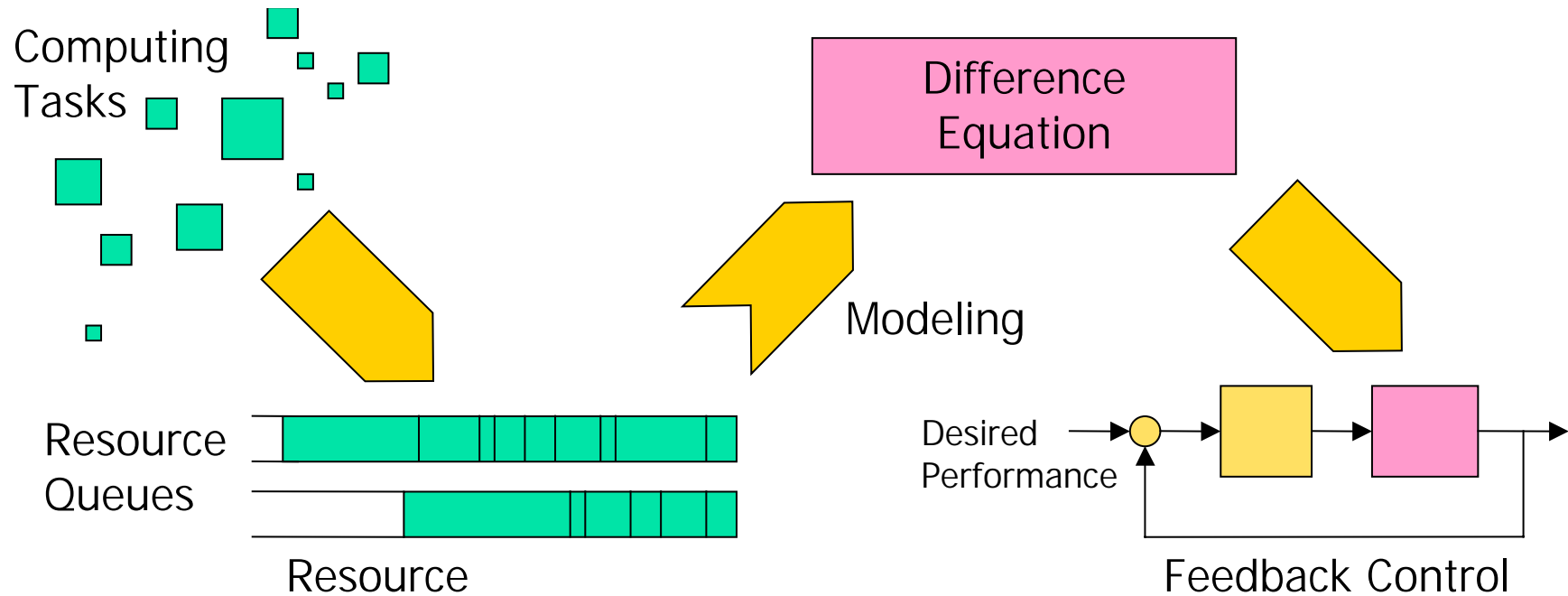
# Processes with deadtime

- Examples: transport deadtime in mining, paper, oil, food



# Processes with deadtime

- Example: resource allocation in computing



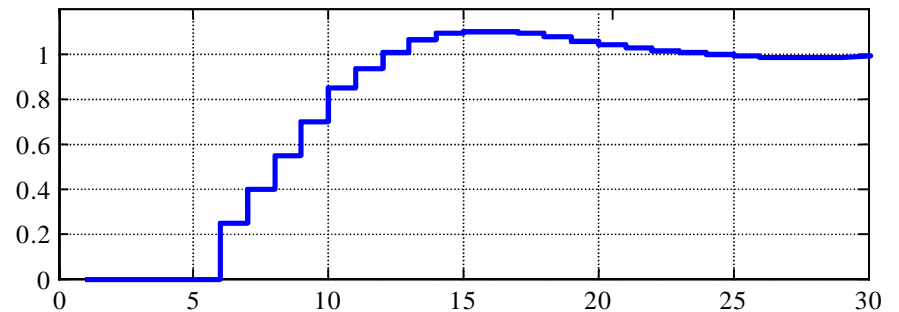
# Control of process with deadtime

- PI control of a deadtime process

$$P = e^{-sT_D} \quad \text{continuous time}$$

$$P = z^{-d} \quad \text{discrete time}$$

PLANT:  $P = z^{-5}$  ; PI CONTROLLER:  $k_p = 0.3, k_i = 0.2$



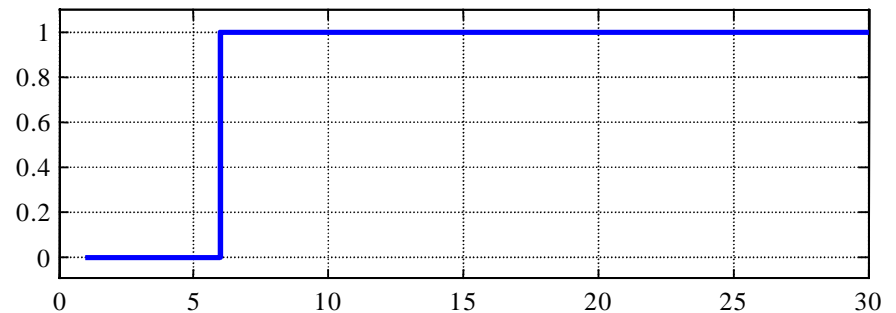
- Can we do better?

- Make  $\frac{PC}{1+PC} = z^{-d}$

- Deadbeat controller

$$PC = \frac{z^{-d}}{1 - z^{-d}} \implies C = \frac{1}{1 - z^{-d}}$$

DEADBEAT CONTROL



$$u(t) = u(t-d) + e(t)$$

# Model-reference control

- Deadbeat control has bad robustness, especially w.r.t. deadtime
- More general model-reference control approach
  - make the closed-loop transfer function as desired

$$\frac{P(z)C(z)}{1 + P(z)C(z)} = Q(z)$$

$$C(z) = \frac{1}{P(z)} \cdot \frac{Q(z)}{1 - Q(z)}$$

- Works if  $Q(z)$  includes a deadtime, at least as large as in  $P(z)$

# Dahlin's controller

- Eric Dahlin worked for IBM in San Jose (?) then for Measurex in Cupertino.
- Dahlin's controller, 1968

$$C(z) = \frac{1}{P(z)} \cdot \frac{Q(z)}{1-Q(z)}$$

$$P(z) = \frac{g(1-b)}{1-bz^{-1}} z^{-d}$$

- plant, generic first order response with deadtime

$$Q(z) = \frac{1-\alpha}{1-\alpha z^{-1}} z^{-d}$$

- reference model

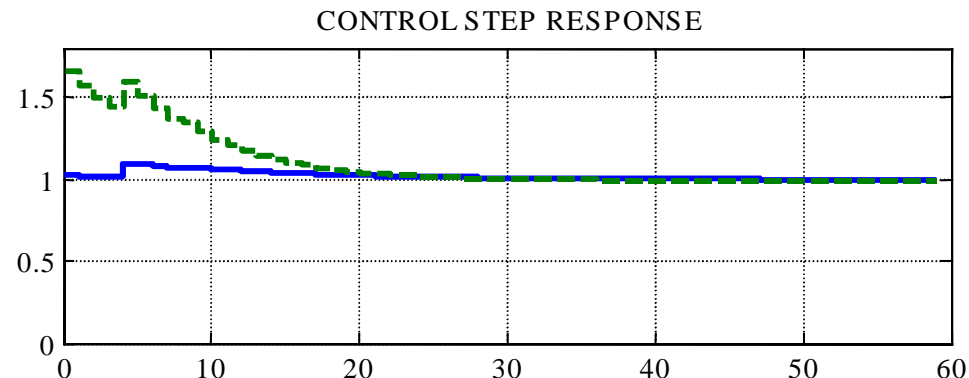
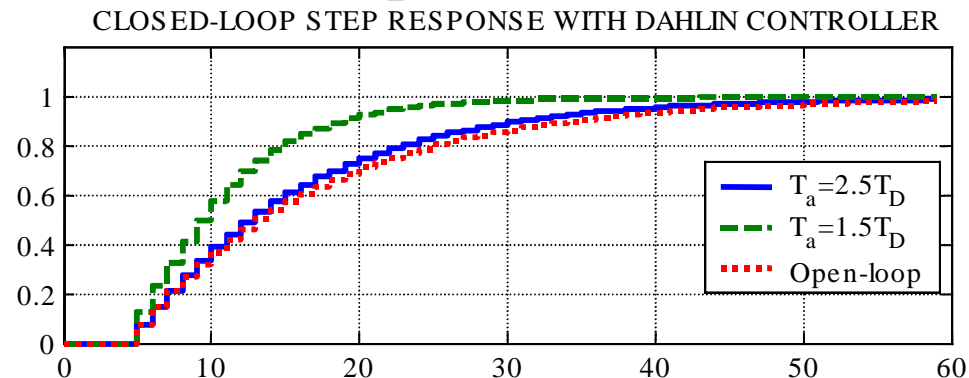
$$C(z) = \frac{1-bz^{-1}}{g(1-b)} \cdot \frac{1-\alpha}{1-\alpha z^{-1} - (1-\alpha)z^{-d}}$$

- Dahlin's controller

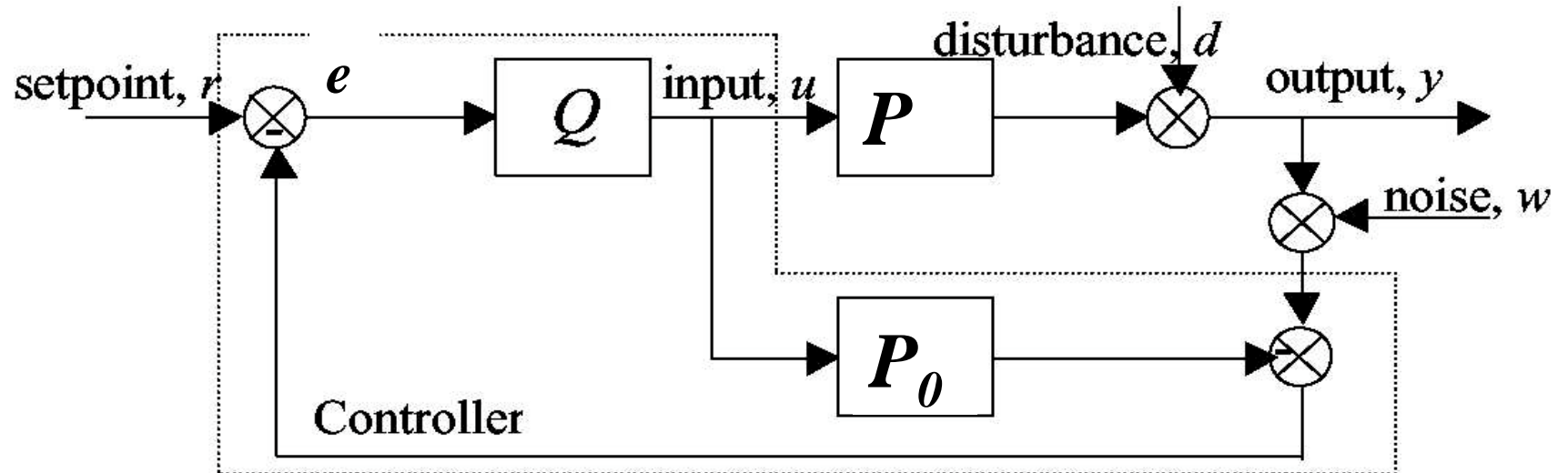
- Single tuning parameter:  $\alpha$  - tuned controller

# Dahlin's controller

- Dahlin's controller is broadly used through paper industry in supervisory control loops - Honeywell-Measurex, 60%.
- Direct use of the identified model parameters.
- Industrial tuning guidelines:  
Closed loop time constant = 1.5-2.5  
deadtime.

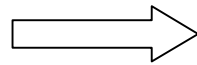


# Internal Model Control - IMC



$$e = r - (y - Pu)$$

$$u = Qe$$



$$C = \frac{Q}{1 - QP_0}$$

- continuous time  $s$
- discrete time  $z$



# IMC and Youla parametrization

- Sensitivities

$$C = \frac{Q}{1 - QP_0}$$

$$\begin{array}{l} \downarrow \\ S = 1 - QP_0 \quad d \rightarrow y \\ T = QP_0 \quad r \rightarrow y \\ S_u = Q \quad d \rightarrow u \end{array}$$

$$Q = \frac{C}{1 + CP_0}$$

- If  $Q$  is stable, then  $S$ ,  $T$ , and the loop are stable
- If loop is stable, then  $Q$  is stable

- Choosing various stable  $Q$  parameterizes all stabilizing controllers
- This is called Youla parameterization
- Youla parameterization is valid for unstable systems as well

# Q-loopshaping

- Systematic controller design: select  $Q$  to achieve the tradeoff
- The approach used in modern advanced control design:  $H_2/H_\infty$ , LMI,  $H_\infty$  loopshaping

- $Q$ -based loopshaping:

$$S = 1 - QP_0 \quad S \ll 1 \Rightarrow Q \approx (P_0)^{-1} \quad \bullet \text{ in band}$$

- Recall system inversion



# Q-loopshaping

- Loopshaping

$$\begin{array}{ll}
 S = 1 - QP_0 & S \ll 1 \Rightarrow Q \approx (P_0)^{-1} \\
 T = QP_0 & T \ll 1 \Rightarrow QP_0 \ll 1
 \end{array}$$

- in band
- out of band

- Lambda-tuned IMC †

$$\begin{array}{l}
 Q = FP_0^\dagger, \quad S = 1 - QP_0 \approx 1 - F \\
 F = \frac{1}{(1 + \lambda s)^n}
 \end{array}$$

Loopshaping

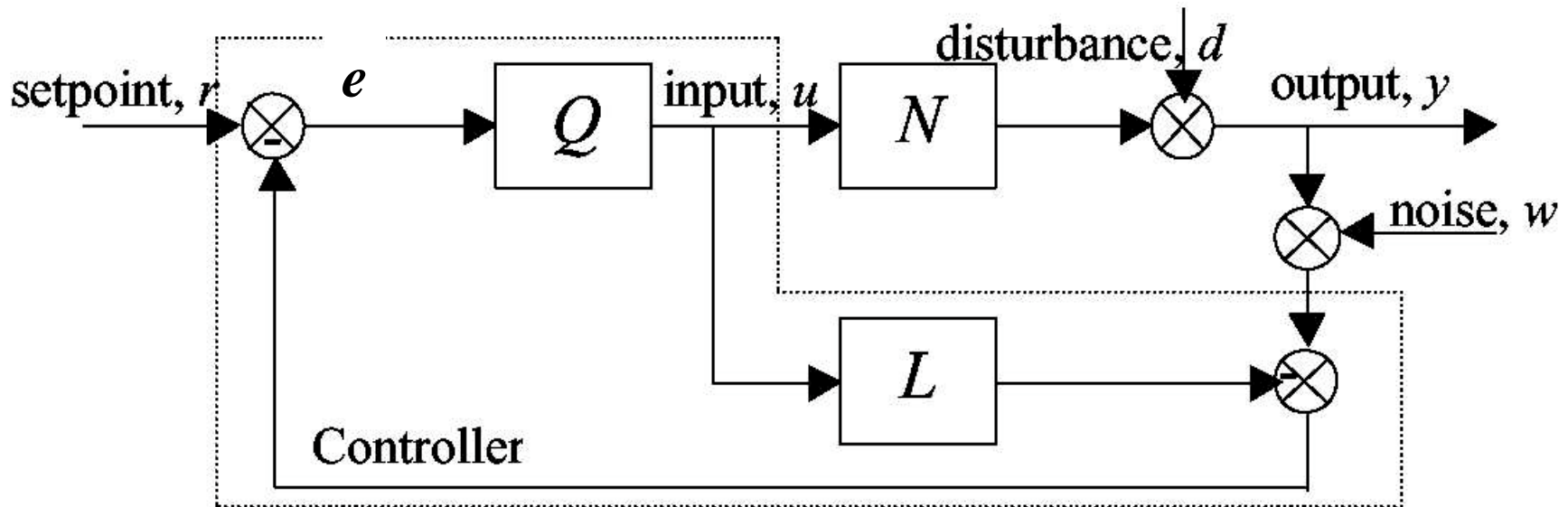
- $F$  is called IMC filter,  $F \approx T$ , reference model for the output
- For minimum phase plant  $Q = FP_0^\dagger = F(P_0)^{-1}$ ,  $T = F$

# IMC extensions

- Multivariable processes
- Nonlinear process IMC
- Dynamic inversion in flight control - Lecture 13 - ?
- Multivariable predictive control - Lecture 12

# Nonlinear process IMC

- Can be used for nonlinear processes
  - linear  $Q$
  - nonlinear model  $P_0$
  - linearized model  $L$



# Industrial applications of IMC

- Multivariable processes with complex dynamics
- Demonstrated and implemented in process control by academics and research groups in very large corporations.
- Not used commonly in process control (except Dahlin controller)
  - detailed analytical models are difficult to obtain
  - field support and maintenance
    - process changes, need to change the model
    - actuators/sensors off
    - add-on equipment

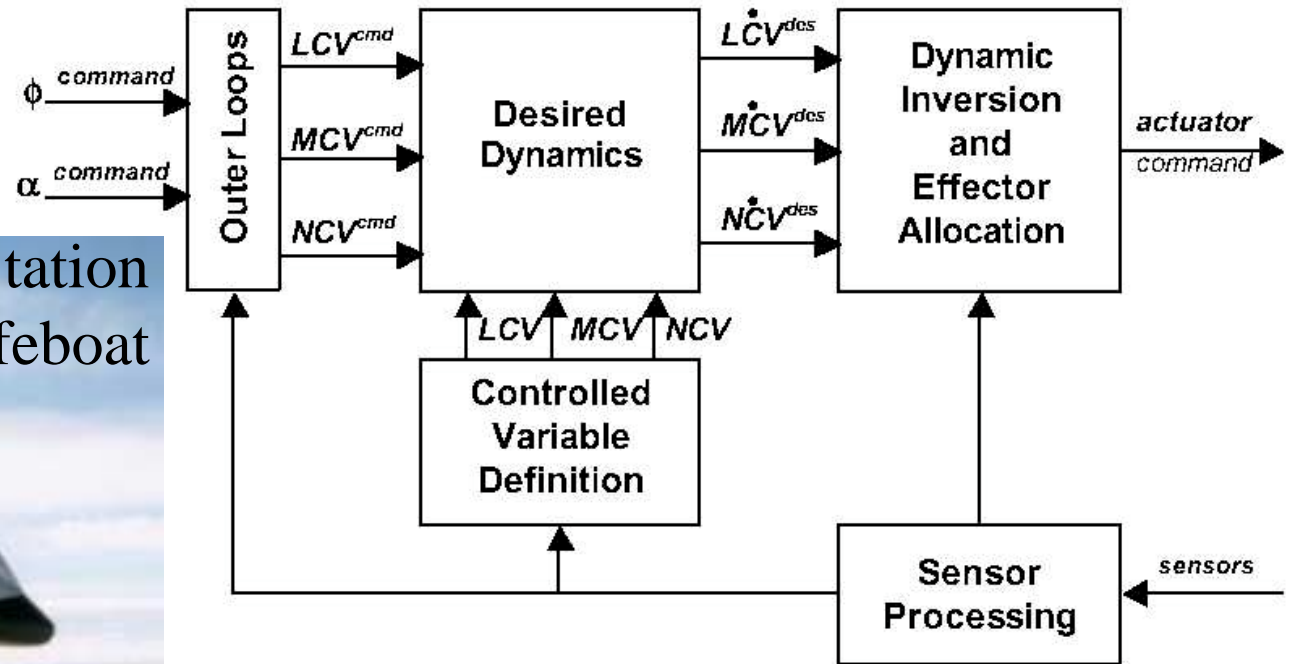
# Dynamic inversion in flight control

$$\dot{v} = F(x, v) + G(x, v)u$$

$$u = G^{-1}(\dot{v}^{des} - F)$$

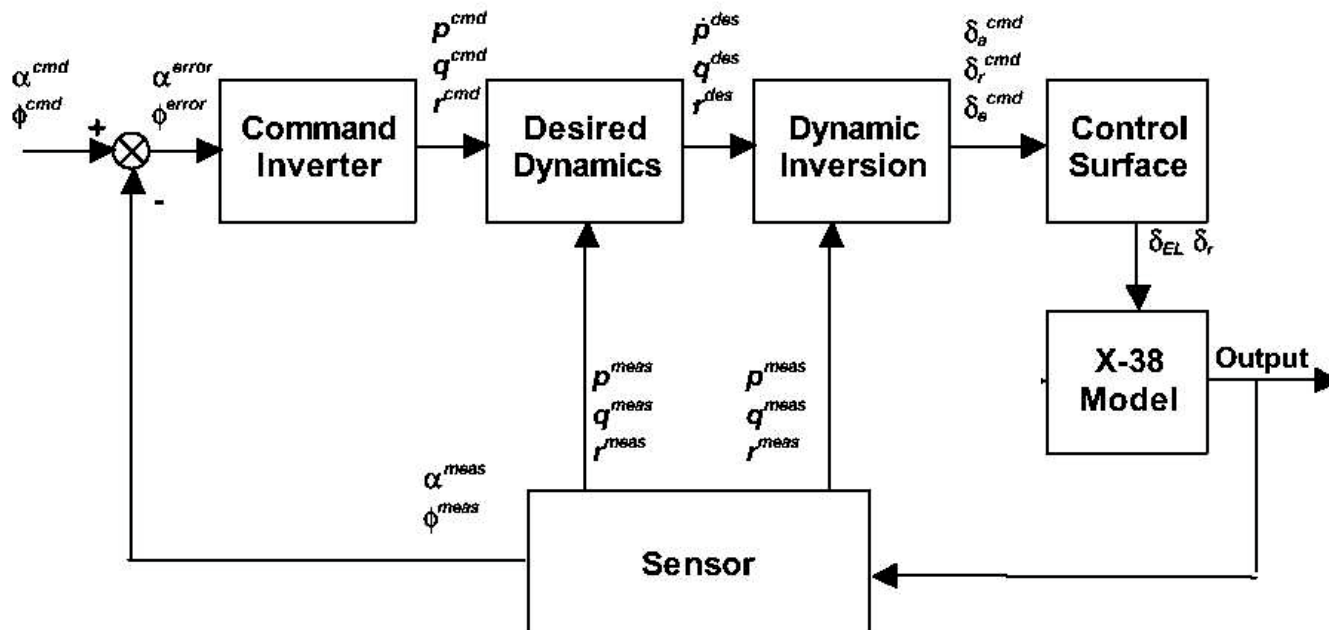
$$v = \begin{bmatrix} LCV \\ MCV \\ NCV \end{bmatrix}$$

- Honeywell MACH



# Dynamic inversion in flight control

- NASA JSC study for X-38
- Actuator allocation to get desired forces/moments
- Reference model (filter): vehicle handling and pilot 'feel'
- Formal robust design/analysis ( $\mu$ -analysis etc)





# Summary

- Dahlin controller is used in practice
  - easy to understand and apply
- IMC is not really used much
  - maintenance and support issues
- Youla parameterization is used as a basis of modern advanced control design methods.
  - Industrial use is very limited.
- Dynamic inversion is used for high performance control of air and space vehicles
  - this was presented for breadth, the basic concept is simple
  - need to know more of advanced control theory to apply in practice